



**<sup>●</sup> http://www.tcm.phy.cam.ac.uk/~bm418/** 

# *Ionic conductors Lecture 9*

Bartomeu Monserrat Course B: Materials for Devices







# **Ionic motion in crystals**



# **Site jump**







# **Yttria-stabilised zirconia (YSZ)**



- ‣ Yttria-stabilised zirconia
- ‣ Oxygen vacancies mediate ionic conduction

### *δ***-Bi2O3**



- $\cdot$   $\delta$ -Bi<sub>2</sub>O<sub>3</sub>
- ‣ Average of 6/8 oxygens per cell
- ‣ Oxygen vacancies mediate ionic conduction

### **Oxygen sensors**







- Electrolyte: conducting through ionic motion but not through electron motion (e.g. YSZ) ‣ Anode: electrical conductor through which current enters the device (e.g. Pt) ‣ Cathode: electrical conductor through which current leaves the device (e.g. Pt)
- 
- 







- ‣ Reference sample: known partial pressure of oxygen
- ‣ Test sample: unknown partial pressure of oxygen



‣ Pt electrodes are porous to let gas through







### Pt(s) | O2(g) (I) | YSZ | O2(g) (II) | Pt(s)





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 $pO_{2}(g)$  (1) <  $pO_{2}(g)$  (11):



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 $pO_2(g)$  (1) <  $pO_2(g)$  (II):

- RHS:  $O_2(g)$  (II) + 4e<sup>-</sup> → 20<sup>2-</sup> reduction (cathode)
- $\cdot$  LHS: 20<sup>2−</sup> → O<sub>2</sub>(g) (I) + 4e<sup>-</sup> oxidation (anode)





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$$
E = -\frac{RT}{4F} \ln \left( \frac{pO_2(I)}{pO_2(II)} \right)
$$

- *E* : electrochemical cell potential [V]
- $R:$  gas constant  $[8.314 \text{ J K}^{-1} \text{mol}^{-1}]$
- *T* : temperature [K]
- *F* : Faraday constant  $[9.649 \times 10^4 \text{ C mol}^{-1}]$





$$
E = -\frac{RT}{4F} \ln \left( \frac{pO_2(I)}{pO_2(II)} \right)
$$

# $\cdot$  If  $pO_2(I) < pO_2(II)$ :  $E > 0$  O<sup>2−</sup>: (II) → (I)  $\cdot$  If  $pO_2(I) > pO_2(II)$ : *E* < 0 0<sup>2−</sup>: (I)→(II)



### **Oxygen sensor**

- ‣ Measure oxygen levels in air for safety
- ‣ Lambda sensor used in vehicle exhaust system





Credit: George McCaa, U.S. Bureau of Mines





‣ Reference gas and exhaust (test) gas



- ‣ Reference gas and exhaust (test) gas
- ‣ YSZ electrolyte in the middle



- ‣ Reference gas and exhaust (test) gas
- ‣ YSZ electrolyte in the middle
- ‣ Permeable Pt electrodes



- ‣ Reference gas and exhaust (test) gas
- ‣ YSZ electrolyte in the middle
- ‣ Permeable Pt electrodes
- ‣ Heater to promote ionic conductivity in YSZ





- ‣ Measures difference between exhaust and atmosphere oxygen partial pressures
- ‣ Linked to fuel injection system to control air/fuel ratio
- ‣ Aim to achieve complete stoichiometric conversion of fuel to minimise emissions:

‣ Non-stoichiometric conversion leads to CO,  $NO_{X_2}$  ...



$$
C_8H_{18} + \frac{25}{2}O_2 \longrightarrow 8CO_2 + 9H_2O
$$



$$
C_8H_{18} + \frac{25}{2}O_2 \longrightarrow 8CO_2 + 9H_2O
$$

‣ From relative molecular masses (remembering air is about  $4N_2$ : $O_2$ ), we get stoichiometric combustion when air-to-fuel ratio by weight is 14.6:

$$
\lambda = \frac{\text{measured ratio}}{14.6}
$$

 $\rightarrow$  Aim for  $\lambda = 1$ 



# cell potential (V) cell potential (V)

oxygen partial pressure (atm) (atm) pressure Dartial oxygen



Fuel rich (burn all oxygen):

oxygen partial pressure (atm) (atm) pressure Jairtial oxygen

- ‣ Low oxygen pressure in exhaust
- 



Lean burn (too little fuel):

oxygen partial pressure (atm) (atm) pressure Idition oxygen

- ‣ High oxygen pressure in exhaust
- 



### **Oxygen pump**





molten metal

- ‣ Aim to purify molten metal
- ‣ Apply external potential to drive oxygen ions from the molten metal to the metal oxide mixture
- ‣ Driving ions from region of low concentration to region of high concentration



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burn fuel (react CH4 with O2)

‣ Gas-fired power station:

**chemical energy**

gas steam spin turbine electricity generator

**thermal energy**



### **electrical energy**

burn fuel (react  $CH_4$  with  $O_2$ )

‣ Gas-fired power station:

**chemical energy**

gas steam spin turbine electricity generator

**thermal energy**

### **mechanical energy**

### **electrical energy**

‣ Fuel cell:

**chemical energy**







- 
- ‣ Anode: porous electrical conductor
- ‣ Cathode: porous conducting material resistant to oxidation

• Electrolyte: conducting through ionic motion but not through electron motion (e.g. YSZ)







### reduction (cathode)

oxidation (anode)







### reduction (cathode)

oxidation (anode)

![](_page_32_Picture_5.jpeg)

# $H_2$  fuel charge CH<sub>4</sub> fuel anode  $| H_2(g) | YSZ | O_2(g) |$  cathode anode  $| CH_4(g) | YSZ | O_2(g) |$  cathode

‣ Overall cell reactions:

‣ Half cell reactions:

$$
O_2 + 4e^- \longrightarrow 2O^{2-}
$$

 $2H_2 + 2O^2$ <sup>-</sup> →  $2H_2O + 4e^-$ 

### $2H_2 + O_2 \longrightarrow 2H_2O$  CH<sub>4</sub> +  $2O_2 \longrightarrow CO_2 + 2H_2O$

 $2O_2 + 8e^ \longrightarrow$  40<sup>2-</sup>

 $CH_4 + 40^{2-} \longrightarrow CO_2 + 2H_2O + 8e^-$ 

![](_page_33_Figure_11.jpeg)

![](_page_34_Figure_1.jpeg)

### **polymer electrolyte membrane**

![](_page_34_Figure_5.jpeg)

![](_page_34_Picture_6.jpeg)

### **yttria-stabilised zirconia electrolyte**

![](_page_34_Picture_3.jpeg)

![](_page_35_Figure_1.jpeg)

- ‣ Polymer electrolyte membrane:
	- Thin and flexible polymer membranes (see Lecture 10)
	- Operate at about 80 °C (cf. YSZ operates at 600-1,000 °C)
	- Conduct protons H +

# °C (cf VSZ onerates at 600-1 000 °

![](_page_35_Picture_7.jpeg)

# anode  $| H_2(g) | YSZ | O_2(g) |$  cathode anode  $| H_2(g) |$  PEM  $| O_2(g) |$  cathode

‣ Overall cell reactions:

### $2H_2 + O_2 \longrightarrow 2H_2O$  2H<sub>2</sub> +  $O_2 \longrightarrow 2H_2O$

‣ Half cell reactions:

$$
O_2 + 4e^- \longrightarrow 2O^{2-}
$$

 $2H_2 + 2O^2$ <sup>-</sup> →  $2H_2O + 4e^-$ 

# YSZ electrolyte **polymer** electrolyte membrane

 $O_2 + 4H^+ + 4e^- \longrightarrow 2H_2O$  $2H_2 \longrightarrow 4H^+ + 4e^-$ 

![](_page_36_Picture_10.jpeg)

### **‣ Advantages:**

- Direct conversion: about twice as efficient as internal combustion engine
- No polluting emissions if fuel is  $H_2$
- No noise (no mechanical parts)

### **‣ Material challenges:**

- 
- Chemically resistant (harsh oxidation and reduction chemical environments)

Matched or low thermal expansion coefficient (high operating temperature)

### **‣ Disadvantages:**

- Hydrogen storage is energy intensive (compress or liquify gas)
- Hydrogen is extremely flammable

### **Hydrogen economy**

![](_page_38_Figure_3.jpeg)

![](_page_38_Picture_4.jpeg)

### hydrogen generation

### $2H_2O \longrightarrow 2H_2 + O_2$

# **Hydrogen economy: challenges**

![](_page_39_Figure_5.jpeg)

hydrogen

generation

### **‣ Hydrogen generation:**

- Splitting water requires energy (electrolysis of water)
- For this to be sustainable, the energy source would ideally be solar energy
- Unsolved problem

# **Hydrogen economy: challenges**

![](_page_40_Figure_5.jpeg)

hydrogen

generation

### **‣ Hydrogen storage:**

- Compressed or liquified gas very energy intensive
- Hydrogen is highly flammable
- Possible solution: using porous materials (e.g. metal-organic frameworks)