



http://www.tcm.phy.cam.ac.uk/~bm418/

# Ionic conductors Lecture 9

Bartomeu Monserrat **Course B: Materials for Devices** 







# **lonic motion in crystals**



# Site jump







# Yttria-stabilised zirconia (YSZ)



- Yttria-stabilised zirconia
- Oxygen vacancies mediate ionic conduction

# $\delta$ -Bi<sub>2</sub>O<sub>3</sub>



- $\delta$ -Bi<sub>2</sub>O<sub>3</sub>
- Average of 6/8 oxygens per cell
- Oxygen vacancies mediate ionic conduction

## Oxygen sensors







- Electrolyte: conducting through ionic motion but not through electron motion (e.g. YSZ) ► Anode: electrical conductor through which current enters the device (e.g. Pt) Cathode: electrical conductor through which current leaves the device (e.g. Pt)







- Reference sample: known partial pressure of oxygen
- Test sample: unknown partial pressure of oxygen





Pt electrodes are porous to let gas through





# $Pt(s) | O_2(g) (I) | YSZ | O_2(g) (II) | Pt(s)$





# $Pt(s) | O_2(g) (I) | YSZ | O_2(g) (II) | Pt(s)$

 $pO_2(g)(I) < pO_2(g)(II)$ :





 $pO_2(g)(I) < pO_2(g)(II)$ :

- RHS:  $O_2(g)(II) + 4e^- \longrightarrow 20^{2-}$
- LHS:  $20^{2-} \rightarrow O_2(g)(I) + 4e^{-1}$

# $Pt(s) | O_2(g) (I) | YSZ | O_2(g) (II) | Pt(s)$

reduction (cathode) oxidation (anode)





# $Pt(s) | O_2(g) (I) | YSZ | O_2(g) (II) | Pt(s)$

 $pO_2(g)(I) < pO_2(g)(II)$ :

- RHS:  $O_2(g)(II) + 4e^- \longrightarrow 20^{2-}$
- LHS:  $20^{2-} \rightarrow O_2(g)(I) + 4e^{-1}$

reduction (cathode) oxidation (anode)





$$E = -\frac{RT}{4F} \ln\left(\frac{pO_2(I)}{pO_2(II)}\right)$$

- *E* : electrochemical cell potential [V]
- $R: gas constant [8.314 J K^{-1} mol^{-1}]$
- T: temperature [K]
- F: Faraday constant  $[9.649 \times 10^4 \,\mathrm{C}\,\mathrm{mol}^{-1}]$





$$E = -\frac{RT}{4F} \ln\left(\frac{pO_2(I)}{pO_2(II)}\right)$$

# If $pO_2(I) < pO_2(II)$ : E > 0 O<sup>2−</sup>: (II)→(I) If $pO_2(I) > pO_2(II)$ : E < 0 O<sup>2−</sup>: (I)→(II)



# Oxygen sensor

- Measure oxygen levels in air for safety
- Lambda sensor used in vehicle exhaust system





Credit: George McCaa, U.S. Bureau of Mines





Reference gas and exhaust (test) gas



- Reference gas and exhaust (test) gas
- YSZ electrolyte in the middle



- Reference gas and exhaust (test) gas
- YSZ electrolyte in the middle
- Permeable Pt electrodes



- Reference gas and exhaust (test) gas
- YSZ electrolyte in the middle
- Permeable Pt electrodes
- Heater to promote ionic conductivity in YSZ ►





- Measures difference between exhaust and atmosphere oxygen partial pressures
- Linked to fuel injection system to control air/fuel ratio
- Aim to achieve complete stoichiometric conversion of fuel to minimise emissions:

$$C_8H_{18} + \frac{25}{2}O_2 \longrightarrow 8CO_2 + 9H_2O$$

 Non-stoichiometric conversion leads to CO, NO<sub>x</sub>, ...





$$C_8H_{18} + \frac{25}{2}O_2 \longrightarrow 8CO_2 + 9H_2O$$

 From relative molecular masses (remembering air is about 4N<sub>2</sub>:O<sub>2</sub>), we get stoichiometric combustion when air-to-fuel ratio by weight is 14.6:

$$\lambda = \frac{\text{measured ratio}}{14.6}$$

• Aim for  $\lambda = 1$ 

![](_page_22_Figure_6.jpeg)

![](_page_23_Picture_1.jpeg)

# cell potential (V)

(atm) pressure partial oxygen

![](_page_24_Figure_1.jpeg)

Fuel rich (burn all oxygen):

- Low oxygen pressure in exhaust
- High cell potential

(atm) pressure partial oxygen

![](_page_25_Figure_1.jpeg)

Lean burn (too little fuel):

- High oxygen pressure in exhaust
- Low cell potential

(atm) pressure partial oxygen

# Oxygen pump

![](_page_26_Figure_1.jpeg)

![](_page_26_Figure_2.jpeg)

molten metal

- Aim to purify molten metal
- Apply external potential to drive oxygen ions from the molten metal to the metal oxide mixture
- Driving ions from region of low concentration to region of high concentration

![](_page_27_Figure_0.jpeg)

- Aim to purify molten metal
- Apply external potential to drive oxygen ions from the molten metal to the metal oxide mixture
- Driving ions from region of low concentration to region of high concentration

Gas-fired power station:

chemical energy

thermal energy

burn fuel (react CH<sub>4</sub> with O<sub>2</sub>)

gas steam

### electrical energy

electricity generator

![](_page_28_Picture_9.jpeg)

spin turbine

Gas-fired power station:

chemical energy

thermal energy

burn fuel (react CH<sub>4</sub> with O<sub>2</sub>)

gas steam

Fuel cell:

chemical energy

![](_page_29_Figure_9.jpeg)

### electrical energy

electricity generator

### mechanical energy

spin turbine

![](_page_29_Picture_14.jpeg)

![](_page_30_Figure_1.jpeg)

- Anode: porous electrical conductor
- Cathode: porous conducting material resistant to oxidation

Electrolyte: conducting through ionic motion but not through electron motion (e.g. YSZ)

![](_page_30_Picture_7.jpeg)

![](_page_31_Figure_1.jpeg)

![](_page_31_Figure_2.jpeg)

### reduction (cathode)

 $0 + 4e^{-}$  oxidation (anode)

![](_page_31_Picture_5.jpeg)

![](_page_32_Figure_1.jpeg)

![](_page_32_Figure_2.jpeg)

### reduction (cathode)

+ 8e<sup>-</sup> oxidation (anode)

![](_page_32_Picture_5.jpeg)

# H<sub>2</sub> fuel anode $|H_2(g)|YSZ|O_2(g)|$ cathode

• Overall cell reactions:

### $2H_2 + O_2 \longrightarrow 2H_2O$

Half cell reactions:

$$O_2 + 4e^- \longrightarrow 20^{2-}$$

 $2H_2 + 2O^{2-} \longrightarrow 2H_2O + 4e^{-}$ 

# CH<sub>4</sub> fuel anode $|CH_4(g)|YSZ|O_2(g)|$ cathode

### $CH_4 + 2O_2 \longrightarrow CO_2 + 2H_2O_2$

### $20_2 + 8e^- \longrightarrow 40^{2-}$

 $CH_4 + 4O^{2-} \longrightarrow CO_2 + 2H_2O + 8e^{-1}$ 

![](_page_33_Figure_11.jpeg)

![](_page_34_Figure_1.jpeg)

### yttria-stabilised zirconia electrolyte

![](_page_34_Picture_3.jpeg)

### polymer electrolyte membrane

![](_page_34_Figure_5.jpeg)

![](_page_34_Picture_6.jpeg)

![](_page_35_Figure_1.jpeg)

- Polymer electrolyte membrane:
  - Thin and flexible polymer membranes (see Lecture 10)
  - Operate at about 80 °C (cf. YSZ operates at 600-1,000 °C)
  - Conduct protons H<sup>+</sup>

### s (see Lecture 10) es at 600-1,000 °C)

![](_page_35_Picture_7.jpeg)

# YSZ electrolyte anode $|H_2(g)|YSZ|O_2(g)|$ cathode

• Overall cell reactions:

### $2H_2 + O_2 \longrightarrow 2H_2O$

Half cell reactions:

$$O_2 + 4e^- \longrightarrow 20^{2-}$$

 $2H_2 + 2O^{2-} \longrightarrow 2H_2O + 4e^{-}$ 

# polymer electrolyte membrane anode $|H_2(g)|$ PEM $|O_2(g)|$ cathode

### $2H_2 + O_2 \longrightarrow 2H_2O$

 $O_2 + 4H^+ + 4e^- \longrightarrow 2H_2O$  $2H_2 \longrightarrow 4H^+ + 4e^-$ 

![](_page_36_Picture_10.jpeg)

### Advantages:

- Direct conversion: about twice as efficient as internal combustion engine
- No polluting emissions if fuel is H<sub>2</sub>
- No noise (no mechanical parts)

### **Disadvantages:**

- Hydrogen storage is energy intensive (compress or liquify gas) ----
- Hydrogen is extremely flammable

### Material challenges:

- Chemically resistant (harsh oxidation and reduction chemical environments)

Matched or low thermal expansion coefficient (high operating temperature)

# Hydrogen economy

### hydrogen generation

### $2H_2O \longrightarrow 2H_2 + O_2$

![](_page_38_Figure_3.jpeg)

![](_page_38_Picture_4.jpeg)

# Hydrogen economy: challenges

### Hydrogen generation:

- Splitting water requires energy (electrolysis of water)
- For this to be sustainable, the energy source would ideally be solar energy
- Unsolved problem

![](_page_39_Figure_5.jpeg)

hydrogen

generation

# olysis of water) source would ideally be solar energy

# Hydrogen economy: challenges

### Hydrogen storage:

- Compressed or liquified gas very energy intensive
- Hydrogen is highly flammable
- Possible solution: using porous materials (e.g. metal-organic frameworks)

![](_page_40_Figure_5.jpeg)

hydrogen

generation